

Document made available under the Patent Cooperation Treaty (PCT)

International application number: PCT/FI05/000010

International filing date: 10 January 2005 (10.01.2005)

Document type: Certified copy of priority document

Document details: Country/Office: FI
Number: 20040046
Filing date: 15 January 2004 (15.01.2004)

Date of receipt at the International Bureau: 16 March 2005 (16.03.2005)

Remark: Priority document submitted or transmitted to the International Bureau in compliance with Rule 17.1(a) or (b)



World Intellectual Property Organization (WIPO) - Geneva, Switzerland
Organisation Mondiale de la Propriété Intellectuelle (OMPI) - Genève, Suisse

Helsinki 24.2.2005

ETUOIKEUSTODISTUS
PRIORITY DOCUMENT



Hakija
Applicant

Outokumpu Oyj
Espoo

Patenttihakemus nro
Patent application no

20040046

Tekemispäivä
Filing date

15.01.2004

Kansainvälinen luokka
International class

F27D

Keksinnön nimitys
Title of invention

"Supply system for suspension smelting furnace"
(Suspensiosulatusuunin syöttöjärjestelmä)

Täten todistetaan, että oheiset asiakirjat ovat tarkkoja jäljennöksiä Patentti- ja rekisterihallitukselle alkuaan annetuista selityksestä, patenttivaatimuksista, tiivistelmästä ja piirustuksista.

This is to certify that the annexed documents are true copies of the description, claims, abstract and drawings, originally filed with the Finnish Patent Office.

Marketta Tehikoski
Apulaistarkastaja

Maksu 50 €
Fee 50 EUR

Maksu perustuu kauppa- ja teollisuusministeriön antamaan asetukseen 1142/2004 Patentti- ja rekisterihallituksen maksullisista suoritteista muutoksineen.

The fee is based on the Decree with amendments of the Ministry of Trade and Industry No. 1142/2004 concerning the chargeable services of the National Board of Patents and Registration of Finland.

Osoite: Arkadiankatu 6 A Puhelin: 09 6939 500 Telefax: 09 6939 5328
P.O.Box 1160 Telephone: + 358 9 6939 500 Telefax: + 358 9 6939 5328
FI-00101 Helsinki, FINLAND

SUPPLY SYSTEM FOR SUSPENSION SMELTING FURNACE

This invention relates to a supply system for supplying a suspension smelting furnace with a feed of fine-grained material. Particularly, the invention relates to
5 a method and an installation of feeding metal concentrate containing fine-grained material in a burner of a suspension smelting furnace.

Suspension smelting is a method of producing matte or metal from finely divided metal concentrates, such as copper, nickel or lead concentrates.
10 Typically, a suspension smelting furnace comprises a round vertical reaction shaft for roasting and smelting dried concentrate in suspension; a settling hearth for collecting the molten droplets and separating matte or metal from slag; and an uptake shaft for waste gas and flue dust.

15 The smelting of the metal concentrate mainly takes place in the vertical reaction shaft. The metal concentrate, oxygen enriched air, and slag-forming agent, i.e. flux, is fed into the reaction shaft via the top part of the shaft.

Various sorts of concentrates and fluxes are mixed and dried in a rotary dryer, a
20 steam drier or a flash dryers. The dried feed is conveyed to the top of the reaction shaft, where the concentrate burner is mounted. Several different types of concentrate burners have been developed to advantageously realize the reactions between the solids and gas in the reaction shaft.

25 Suspension smelting is a high-capacity method of refining metal concentrates. Production capacity of a modern suspension smelting furnace can be characterized by daily concentrate throughput which is in the range of several thousands (2000 – 5000) of tons of dried concentrate. In running a modern suspension smelting furnace, it is essential that the utilization rate is kept high.
30 The target is to continuously maintain full operation of the furnace for hundreds of hours. Unnecessary down time can be reduced ensuring a continuous and

reliable operation of the concentrate feeding system for the burner of the smelting furnace.

Known approach to solve the problem of providing a continuous and reliable
5 feed of concentrate into the burner is to construct an intermediate storage bin for the concentrate close to the burner on the level of the top of the reaction shaft. Constant feed rate is realized with a feeding control unit arranged between the storage bin and the burner. Dried concentrate may be lifted with a
10 pneumatic conveyor into the storage bin. The charge of the intermediate storage bin should approximately correspond to a three- or four- hours feed of the suspension furnace, i.e. 100 – 600 tons of concentrate. As the height of the furnace exceeds 20 meters, the construction of the intermediate bin becomes heavy and requires high investment.

- 15 The present invention solves the problem described above and provides an improved method and installation for providing a burner of a suspension smelting furnace with reliable and continuous concentrate feed. The invention is based on the idea that the heavy construction of concentrate bin is located below the level of the top of the reaction shaft, i.e. close to the ground level.
20 More particularly, the outlet of the concentrate bin is located below the level of the top of the reaction shaft and close to the ground level.

The feed of the burner is fine-grained matter and comprises dried mixture of concentrate and flux and most often also flue dust. In a suspension smelter, it
25 is common practice to recycle flue dust recovered from the exhaust gas. The feed is conveyed on the top level of the reaction shaft with a pneumatic conveyor. The feed rate is controlled with a feed rate controller that is adapted between the storage bin and the pneumatic conveyor.

- 30 Remarkable advantages are reached by aid of the present invention. The installation for feeding concentrate mixture into a suspension smelting furnace is simple and the construction becomes lighter. Further, the installation and the

method of the present invention requires lower investments than the constructions presently in use. The installation and the method eliminate incident interruptions of the feed from a concentrate direr.

- 5 The installation of the present invention provides a concentrate burner of a suspension smelting furnace with continuous and constant feed of fine-grained matter. The concentrate burner is adapted on top of a reaction shaft of a suspension smelting furnace. The installation of the present invention comprises a bin having an inlet and outlet for the fine-grained matter; a feed
10 control unit for providing the feed of the particulate matter with accurately controlled feed rate; and a pneumatic conveyor adapted to transport the particulate matter up to the top level of the suspension smelting furnace. The outlet of the bin for the fine-grained matter locates essentially at lower level than the top of the reaction shaft. The feed control unit is adapted to receive
15 fine-grained matter from the outlet of the bin and to provide the pneumatic conveyor with the feed of the particulate matter. The pneumatic conveyor is adapted to provide the concentrate burner with a feed rate that equals with the feed rate provided by the feed control unit.
- 20 The method of the present invention provides a concentrate burner that is adapted on top of a reaction shaft of a suspension smelting furnace with an uninterrupted and controlled feed of fine-grained matter comprising metal concentrate. The method comprises steps of feeding fine-grained matter in a bin having an outlet at a lower level than the burner; forming and sustaining in
25 the bin a storage of the fine-grained matter corresponding with at least one hours feed of the suspension smelting furnace; feeding fine-grained matter in a feed rate controller unit that provides the pneumatic conveyor with an uninterrupted and controlled feed of the fine-grained matter; and conveying the matter with the pneumatic conveyor in the burner of the suspension smelting
30 furnace.

The fine-grained matter to be fed into the concentrate burner is a mixture of dried metal concentrate and flux. Further, the feed mixture of a suspension furnace may comprise 3 – 15 % of flue dust recovered from the outlet gas after the uptake shaft of the suspension furnace.

5

According to a preferred embodiment of the present invention the outlet of the concentrate bin is adapted to a loss-in-weight –type feed controller. The operation and principles of a loss-in-weight feeder is described in US 6,446,836. The feed controller is adapted to feed the concentrate into a dilute -
10 phase pneumatic conveyor. The density of the transported fine-grained matter is 10 – 50 kg solid material / 1 kg air and the conveying pressure is normally between 1 and 3 bar. The pneumatic conveyor lifts the particulate matter on top of the reaction shaft and the pneumatic conveyor is adapted to feed the material straight into the concentrate burner. The feed rate into the concentrate
15 burner equals with the feed rate provided by the feed controller.

According to another preferred embodiment of the present invention the outlet of the concentrate bin is adapted to a feed controller of a dense-phase pneumatic conveyor. The pressure in the pneumatic conveyor and in the feed
20 controller unit of the conveyor is around 6 bar. The density of the transported fine-grained matter is 50 – 150 kg solid material / 1 kg air. The pneumatic conveyor is adapted to feed fine-grained matter straight into the concentrate burner.

25 According to one more embodiment of the present invention the outlet of the concentrate bin is adapted to a loss-in-weight –type feed controller. The feed controller is adapted to feed the concentrate into an air-lift –type pneumatic conveyor. The pressure in the air-lift is around 0.3 bar. The air-lift conveyor is provided with an expansion vessel where most of the compressed air is
30 separated from the solid. The solid is fed via an air-lock feeder in to an air-slide-type conveyor, which is adapted to feed the concentrate into the concentrate

burner. The mass flow provided by the air-slide conveyor is adapted to equal with the feed rate provided by the loss-in-weight controller.

Fig. 1 is a schematic presentation of an installation of a preferred embodiment of the present invention.

Fig. 2 is a schematic presentation of an installation of another preferred embodiment of the present invention.

Fig. 3 is a schematic presentation of an installation of one more embodiment of the present invention.

10

In the installation of Fig. 1, dried mixture of metal concentrate and fluxing agent is fed via pipe 48 into a bin 10. The outlet 46 of the bin is adapted to feed the concentrate mixture into a loss-in-weight feed controller 11. A screw conveyor 14 conveys an accurate mass flow of the concentrate mixture into a pneumatic conveyor 12, which is a dilute-phase pneumatic conveyor. The pneumatic conveyor 12 lifts the concentrate mixture up to the concentrate burner 13 of the suspension smelting furnace 16. As shown in Fig. 1, the outlet 46 of the bin 10 is located at essentially lower level than the top of the reaction shaft 15 and the concentrate burner 13. Flue dust is fed into a bin 17. The feed ratio of the concentrate mixture and the flue dust has to be carefully controlled. Therefore, the flue dust is fed into a feed rate controller 18 and the controlled mass flow of the flue dust is conveyed via a screw conveyor 19 into the pneumatic conveyor 12. The flow of the concentrate mixture and the flue dust is continuous and thus ensures unbreakable operation of the suspension smelting furnace 16.

25

Fig. 2 shows that dried mixture of metal concentrate and fluxing agent is fed via pipe 47 into a bin 20. The outlet 45 of the bin is adapted to feed the concentrate mixture into an intermediate pressure chamber 24 for loading the feed controller 21 of the pneumatic conveyor 22. The pneumatic conveyor 22 is a dense-phase pneumatic conveyor. An accurate mass flow of the concentrate mixture is fed into the pneumatic conveyor 22. The pneumatic conveyor 22 lifts the concentrate mixture up to the concentrate burner 23 of the suspension

30

smelting furnace 26. As shown in Fig. 2, the outlet 45 of the bin 20 is located at essentially lower level than the top of the reaction shaft 25 and the concentrate burner 23. Flue dust is fed into a bin 27. The feed ratio of the concentrate mixture and the flue dust is again carefully controlled. Therefore, the flue dust is
 5 fed via a loading chamber 29 into a feed rate controller 28 of a pneumatic conveyor 22 and the controlled mass flow of the flue dust is conveyed with the pneumatic conveyor up to the concentrate burner 23. The flow of the concentrate mixture and the flue dust is continuous and thus ensures unbreakable operation of the suspension smelting furnace 26.

10

Fig. 3 shows that dried mixture of metal concentrate and fluxing agent is fed via pipe 43 into a bin 30. The outlet 44 of the bin is adapted to feed the concentrate mixture into a loss-in-weight feed controller 31 for loading of the pneumatic conveyor 32. The pneumatic conveyor 32 is an air-lift type conveyor. An
 15 accurate mass flow of the concentrate mixture is fed into the pneumatic conveyor 32 via a screw conveyor 34. The pneumatic conveyor 32 lifts the concentrate mixture up to an expansion vessel 40 where the particulate matter is fed via an air-lock feeder on an air-slide conveyor 42. The concentrate burner 33 of the suspension smelting furnace 36 is provided with accurately controlled
 20 and continuous feed. As shown in Fig. 3, the outlet 44 of the bin 30 is located at essentially lower level than the top of the reaction shaft 35 and the concentrate burner 33. Flue dust is fed into a bin 37. The feed ratio of the concentrate mixture and the flue dust is again carefully controlled with the feed rate controllers 31 and 38. Therefore, the flow of the flue dust is controlled with a
 25 loss-in-weight controller 38 and fed via a screw conveyor 39 into the air-lift – type conveyor 32. The flow of the concentrate mixture and the flue dust is continuous and thus ensures unbreakable operation of the suspension smelting furnace 36.

30 The concentrate burners 13, 23, 33 may be of any type of metal concentrate burners. The concentrate burners especially suitable in the installation of the present invention are sleeve type burners and diffuser type burners. The

principle of a sleeve type burner is disclosed in US 6446386, and the principle of a diffuser type burner is disclosed in WO 02/055746.

CLAIMS:

1. An installation for providing a concentrate burner that is adapted on top
5 of a reaction shaft of a suspension smelting furnace with continuous and
constant feed of fine-grained matter, comprising
a bin having an inlet and an outlet for the fine-grained matter;
a feed control unit for providing the feed of the fine-grained matter with
accurately controlled feed rate; and
10 a pneumatic conveyor adapted to transport the fine-grained matter up to
the top level of the suspension smelting furnace;
characterized in that,
the outlet of the bin for the fine-grained matter locates essentially at a
lower level than the top of the reaction shaft;
15 the feed control unit is adapted to receive the fine-grained matter from
the outlet of the bin and to provide the pneumatic conveyor with the feed
of the fine-grained matter; and
the pneumatic conveyor is adapted to provide the concentrate burner
with a feed rate that equals with the feed rate provided by the feed
20 control unit.
2. The installation of claim 1, characterized in that the fine-grained matter
comprises metal concentrate.
- 25 3. The installation of claim 1, characterized in that the fine-grained matter
comprises metal concentrate and fluxing agent.
4. The installation of claim 1, characterized in that the fine-grained matter
comprises metal concentrate, fluxing agent and flue dust.
- 30 5. The installation of claim 1, characterized in that it comprises a first bin
for a dried mixture of metal concentrate and fluxing agent, a second bin

for flue dust, a first feed rate controller for the mixture of metal concentrate and fluxing agent and a second feed rate controller for the flue dust.

- 5 6. The installation of claims 1 – 5, characterized in that the pneumatic conveyor is a dilute-phase pneumatic conveyor.
7. The installation of claims 1 – 5, characterized in that the pneumatic conveyor is a dense-phase pneumatic conveyor.
- 10 8. The installation of claims 1 – 5, characterized in that the pneumatic conveyor is an air-lift type pneumatic conveyor and the air-lift is provided with an expansion vessel adapted to feed the particulate matter into the burner of the suspension smelting furnace via an air-lock feeder and an
- 15 air-slide conveyor.
9. The installation of claims 1 – 5, characterized in that the feed control unit is a loss-in-weight controller and the pneumatic conveyor is a dilute-phase pneumatic conveyor.
- 20 10. The installation of claims 1 – 5, characterized in that the feed control unit is a loss-in-weight controller and the pneumatic conveyor is an air-lift type pneumatic conveyor.
- 25 11. The installation of claims 1 – 5, characterized in that the concentrate burner is a sleeve type burner or a diffusion type burner.
12. A method of providing a concentrate burner, that is adapted on top of a reaction shaft of a suspension smelting furnace, with uninterrupted and controlled feed of fine-grained matter comprising metal concentrate,
- 30 **characterized** in that the method comprises steps of feeding fine-grained matter in a bin having an outlet at a lower level than

the burner;

forming and sustaining in the bin a storage of the fine-grained matter corresponding with at least one hours feed of the suspension smelting furnace;

- 5 feeding fine-grained matter in a feed rate controller unit that provides the pneumatic controller with an uninterrupted and controlled feed of the fine-grained matter; and
- conveying the matter with the pneumatic conveyor in the burner of the suspension smelting furnace.

10

13. The method of claim 12, characterized in that the feed rate controller operates according to the principle of loss-in weight - type controller.

14. The method of claim 12, characterized in that it further comprises a step
- 15 of feeding flue dust into the pneumatic conveyor.

Abstract:

A supply system for providing a suspension smelting furnace with constant and continuous feed is disclosed. The installation of the invention comprises intermediate storage bins for fine-grained feed, a feed rate controller for accurately controlling the feed rate of the fine-grained material, and a pneumatic conveyor for lifting the feed up to the top level of the suspension smelting furnace where the burner of the furnace is adapted. In the installation, the heavy constructions of the storage bins are located close to the ground level and the constructions around and on top of the furnace have been designed essentially lighter than in conventional solutions.

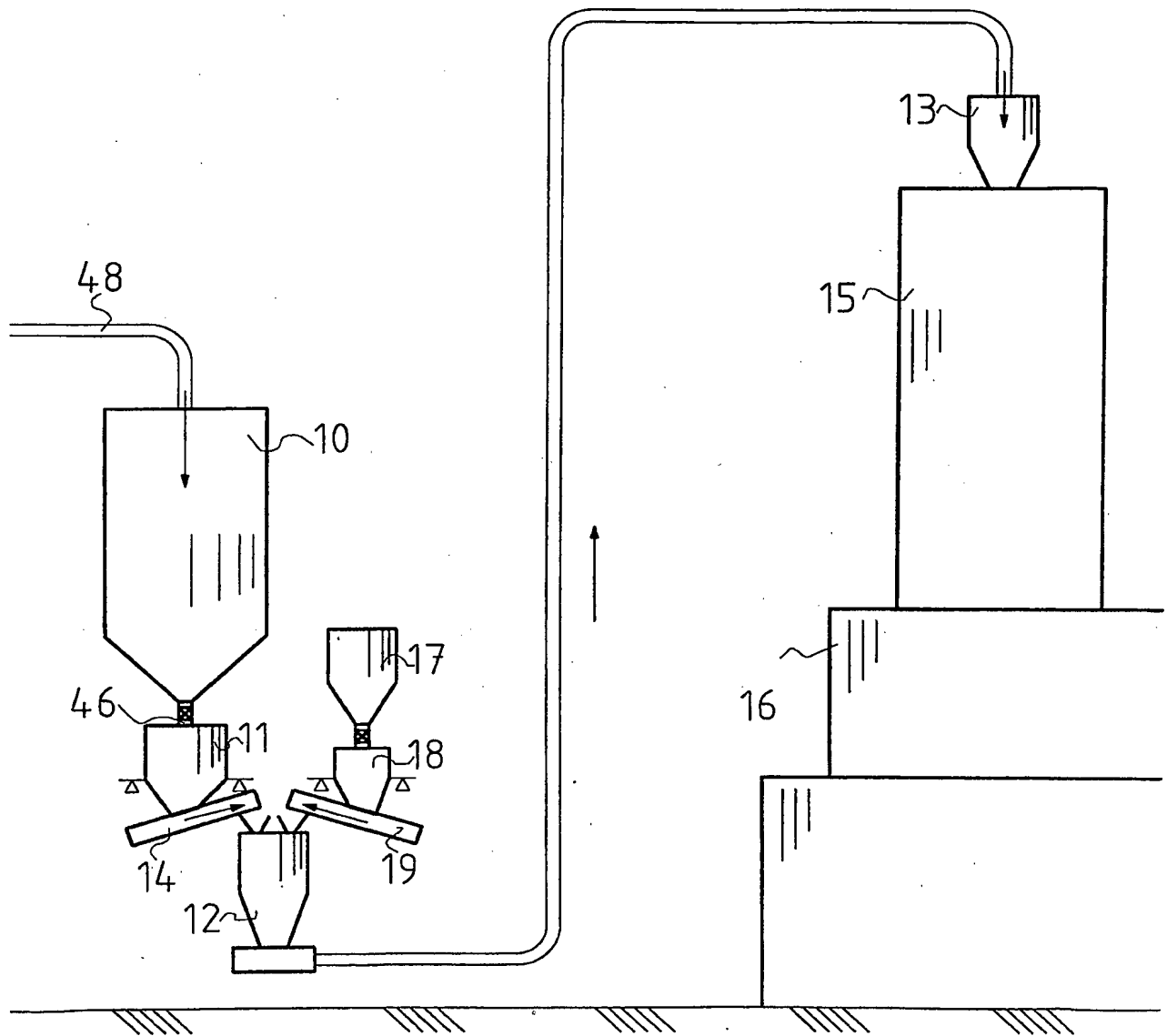


Fig. 1

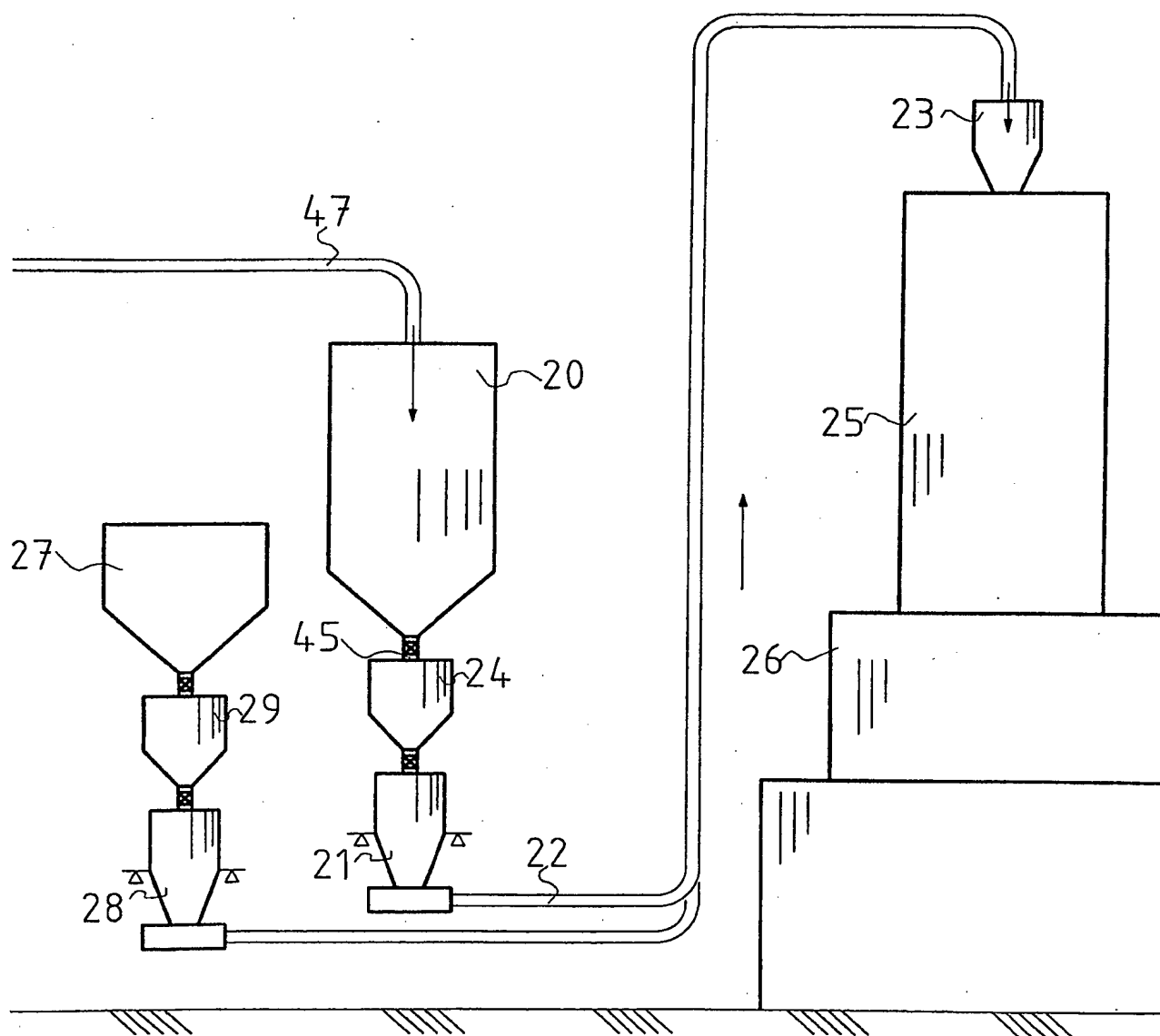


Fig. 2

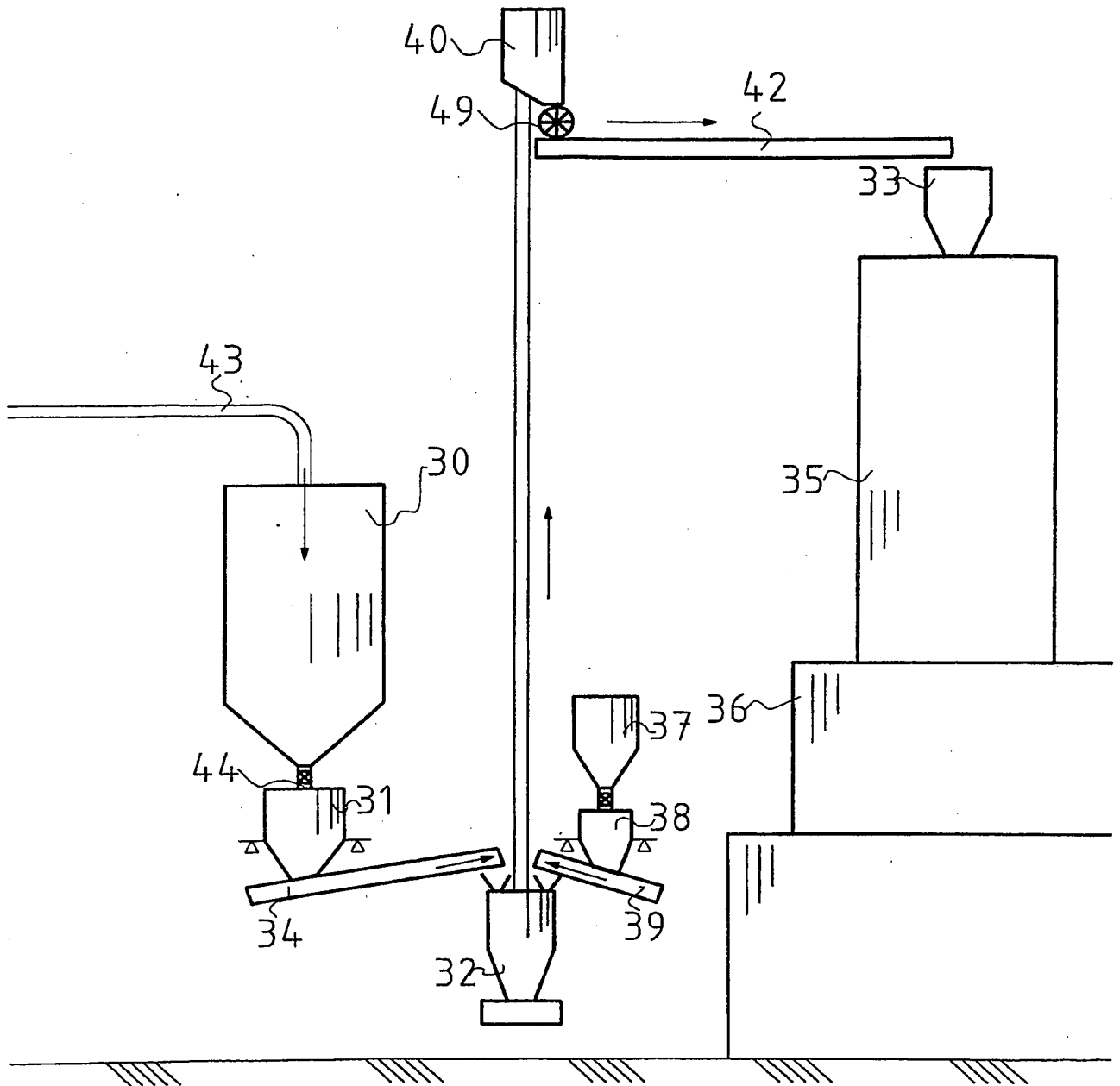


Fig. 3

From the INTERNATIONAL BUREAU

PCTNOTIFICATION CONCERNING
SUBMISSION OR TRANSMITTAL
OF PRIORITY DOCUMENT

(PCT Administrative Instructions, Section 411)

To:

OUTOKUMPU OYJ, INTELLECTUAL PROPERTY
MANAGEMENT
P.O. Box 27
FI-02201 Espoo
FINLANDE

Date of mailing (day/month/year) 17 March 2005 (17.03.2005)	
Applicant's or agent's file reference 20041001 WO	IMPORTANT NOTIFICATION
International application No. PCT/FI05/000010	International filing date (day/month/year) 10 January 2005 (10.01.2005)
International publication date (day/month/year)	Priority date (day/month/year) 15 January 2004 (15.01.2004)
Applicant OUTOKUMPU OYJ et al	

- By means of this Form, which replaces any previously issued notification concerning submission or transmittal of priority documents, the applicant is hereby notified of the date of receipt by the International Bureau of the priority document(s) relating to all earlier application(s) whose priority is claimed. Unless otherwise indicated by the letters "NR", in the right-hand column or by an asterisk appearing next to a date of receipt, the priority document concerned was submitted or transmitted to the International Bureau in compliance with Rule 17.1(a) or (b).
- (If applicable)* The letters "NR" appearing in the right-hand column denote a priority document which, **on the date of mailing of this Form, had not yet been received by the International Bureau** under Rule 17.1(a) or (b). Where, under Rule 17.1(a), the priority document must be submitted by the applicant to the receiving Office or the International Bureau, but the applicant fails to submit the priority document within the applicable time limit under that Rule, **the attention of the applicant is directed** to Rule 17.1(c) which provides that no designated Office may disregard the priority claim concerned before giving the applicant an opportunity, upon entry into the national phase, to furnish the priority document within a time limit which is reasonable under the circumstances.
- (If applicable)* An asterisk (*) appearing next to a date of receipt, in the right-hand column, denotes a priority document **submitted or transmitted to the International Bureau but not in compliance with Rule 17.1(a) or (b)** (the priority document was received after the time limit prescribed in Rule 17.1(a) or the request to prepare and transmit the priority document was submitted to the receiving Office after the applicable time limit under Rule 17.1(b)). Even though the priority document was not furnished in compliance with Rule 17.1(a) or (b), the International Bureau will nevertheless transmit a copy of the document to the designated Offices, for their consideration. In case such a copy is not accepted by the designated Office as the priority document, Rule 17.1(c) provides that no designated Office may disregard the priority claim concerned before giving the applicant an opportunity, upon entry into the national phase, to furnish the priority document within a time limit which is reasonable under the circumstances.

<u>Priority date</u>	<u>Priority application No.</u>	<u>Country or regional Office or PCT receiving Office</u>	<u>Date of receipt of priority document</u>
15 January 2004 (15.01.2004)	20040046	FI	16 March 2005 (16.03.2005)

The International Bureau of WIPO
34, chemin des Colombettes
1211 Geneva 20, Switzerland

Authorized officer

Giffo Schmitt Beate

Facsimile No. +41 22 740 14 35

Facsimile No. +41 22 338 87 20
Telephone No. +41 22 338 9241